



QUANTIFICATION PROTOCOL FOR INSTRUMENT GAS TO INSTRUMENT AIR CONVERSION IN PROCESS CONTROL SYSTEMS

2nd Stage Review of GHG
Quantification Protocols

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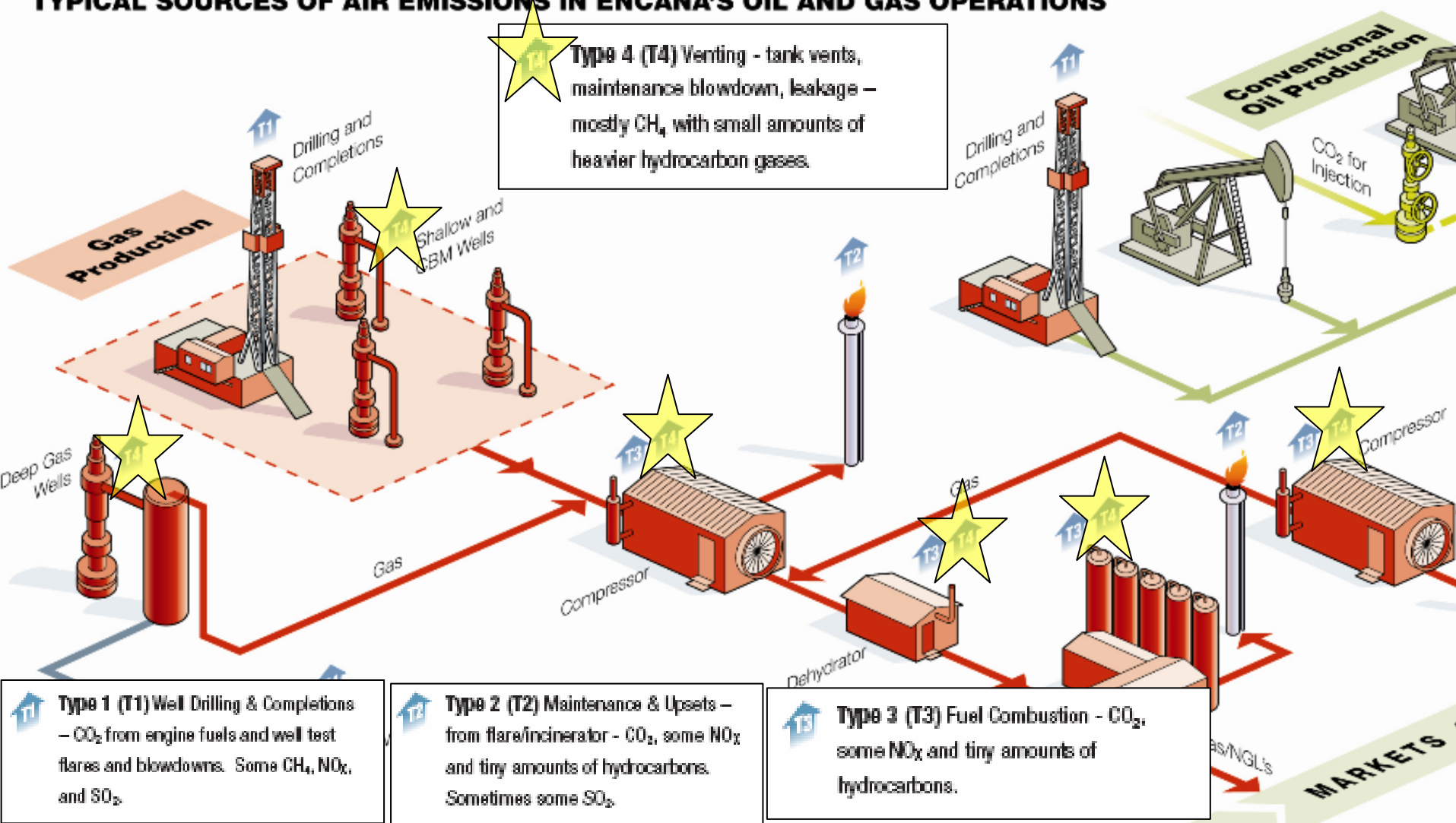
Sutton Place Hotel | Edmonton | December 28, 2008





Introduction

TYPICAL SOURCES OF AIR EMISSIONS IN ENCANA'S OIL AND GAS OPERATIONS





Process Overview

- **Step 1 Alberta Protocol Development Process**
 - **Seed material/key references**
 - Reviewed existing protocols/methodologies
 - US EPA Gas Star Program
 - Instrument Society of America (ISA) Standard
 - ISO 14064 Part 2
 - Industry experts
 - **No directly related protocols available, but some good guidance documents were found**
 - **Developed proposed protocol**



Process Overview

- **Developed TPP and TSD in support of protocol**
- **Expert Technical Review**
 - **Step 7- Alberta Protocol Development Process**
 - Held on November 3rd, 2008
 - Internal/External reviewers-10
 - Industry- BP, EnCana, Petro-Canada
 - Technology providers- Spartan Controls
 - Government- ARC, Climate Change Central
 - Academia- University of Calgary
- **No sustained objections to move forward**
- **Updated protocol with comments from review and feedback submitted one week later.**



Project and Baseline Condition

- **Project Condition**
 - Defined as volume of compressed air used to power pneumatic devices.
 - Compressed air will also need management.
- **Baseline Condition**
 - Defined as the volume of natural gas vented, or flared/combusted to the atmosphere prior to the conversion to the air system.
 - This gas is typically sourced from the fuel supply for the entire facility.
- **Note: Vented gas will be completely eliminated**



Project and Baseline Condition

Baseline

Project

Exhibit 1: Natural Gas Pneumatic Control System

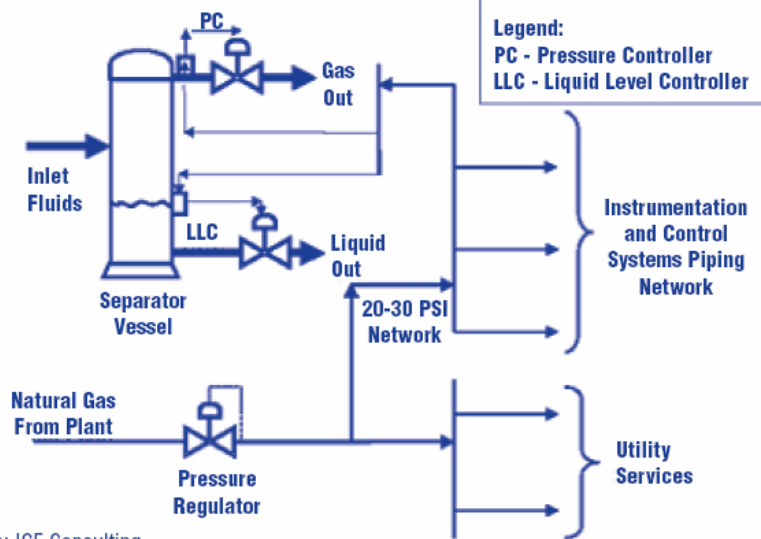
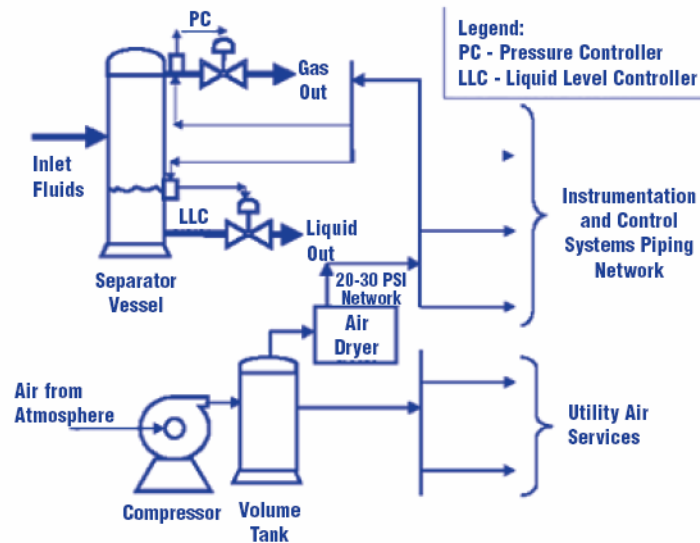


Exhibit 3: Compressed Instrument Air System



Source: US EPA Natural Gas STAR Program (2004). "Lessons Learned- Convert Gas Pneumatic Controls to Instrument Air"



Basis For Reduction

- **Functional Equivalence**
 - Same pressure, different volumes due to nature of gases
 - Metric is volumes of air and gas
 - Multiplied by density, then mass is also metric
- **Emissions reduction are REAL**
 - Elimination of vented or flared/combusted gas
- **Account emissions from air compression and management**
- **Fuel extraction and processing**



Emissions Comparison

- As stated before same volume but different pressure
- Need to compare baseline - project emissions
- Used ISA *ANSI/ISA-75.02-1996 Control Valve Capacity Test Procedures Standard*
 - Made assumptions
- Incorporated gas equivalency formula into protocol

$$Q_{CH_4} = 1.2994 * Q_{AIR}$$



Applicability Criteria

- **Demonstrate functional equivalence-
instrument air will replace instrument gas**
- **Project proponent to inspect and repair leaks
prior to actual metering to reduce and
mitigate risks associated with overestimation
of emissions or use discount factors.**
- **Use section 8.7 in Directive 60-CAPP *Best
Management Practice (BMP) for Fugitive
Emissions Management* to minimize leaks**
- **Instrumentation or Chemical Injection Pumps
(CIP), or other types of equipment.**
- **The project must meet Alberta Offset System
requirements.**



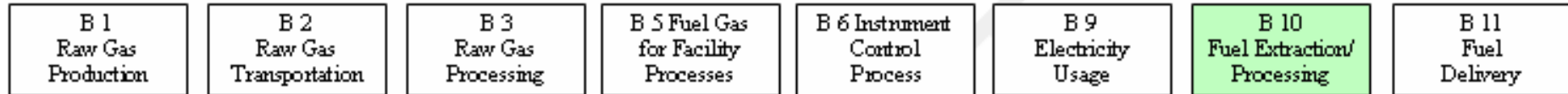
Flexibility Mechanisms

- **Site specific emissions factors may be substituted for generic emission factors (i.e. electricity displacement factor)**
- **Baseline and project metering may be carried out for more than one month**
- **Retroactive crediting for unmetered ongoing projects**
- **Vented and flared/combusted gas streams**
- **Adjustment to baseline by adding or decommissioning of devices**
- **Instrument air conversions can be installed at single or multiple sites-aggregating small projects**



Baseline LCA Analysis-SSs

Upstream SS's During Baseline



Upstream SS's Before Baseline

B 12
Construction on
Site

B 13
Development of
Site

B 14
Building
Equipment

B 15
Transportation
of Equipment

B 16
Testing of
Equipment

On Site SS's During Baseline

B 7
Vented Fuel Gas

B 8 Flared/
Combusted Fuel
Gas

Downstream SS's After Baseline

B 17
Site
Decommissioning

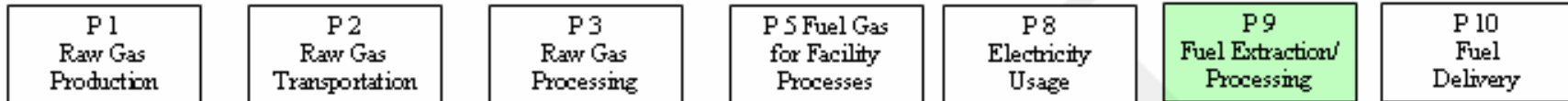
Downstream SS's During Baseline

B 4 Processed
Gas Distribution
and Sale



Project LCA Analysis-SSs

Upstream SS's During Project



Upstream SS's Before Project

P 11
Construction on
Site

P 12
Development of
Site

P 13
Building
Equipment

P 14
Transportation
of Equipment

P 15
Testing of
Equipment

On Site SS's During Project

P 6
Air
Compression

P 7 Air
Management
System

Downstream SS's After Project

P 16
Site
Decommissioning

Downstream SS's During Project

P 4 Processed
Gas Distribution
and Sale



Quantification Approach

$$\text{Emission Reduction} = \text{Emissions}_{\text{Baseline}} - \text{Emissions}_{\text{Project}}$$

$$\text{Emissions}_{\text{Baseline}} = \text{Emissions}_{\text{Fuel Extraction / Processing}} + \text{Emissions}_{\text{Vented Fuel Gas}} + \text{Emissions}_{\text{Flared/Combusted Fuel Gas}}$$

$$\text{Emissions}_{\text{Project}} = \text{Emissions}_{\text{Fuel Extraction / Processing}} + \text{Emissions}_{\text{Air Compression}} + \text{Emissions}_{\text{Air Management System}}$$

- **Key data to be metered (from one month metering as per protocol approach):**
 - Compressed air volumes
 - Electricity for compressor and air management
- **Gases included: CH₄, CO₂, N₂O**



GHG Reduction-Wilson Creek

Baseline Emissions

Vented Gas (46,356 m³/yr or air)	858.4 tCO₂e
Fuel Extraction/Processing	11.5 tCO₂e
Flared/Combusted	-
Total	869.9 tCO₂e

Project Emissions

Air Compression (34,164 kWh/yr)	22.2 tCO₂e
Air Management (2,978 kWh/yr)	1.94 tCO₂e
Total	24.14 tCO₂e
Offsets	845.7 tCO₂e



Thank you for your attention

Questions and suggestions

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Background



Approach- need to compare baseline and project emissions

- **The capacity of a device to flow air or gas is expressed in terms of C_v , or flow coefficient. Measures the impact on flow from diverse factors to a device such as:**
 - Orifice size (diameter of the piping or opening through the valve);
 - Length of piping or opening through the valve;
 - Turbulence caused by bends or turns in the piping;
 - Restrictions, or anything that reduces the orifice size or the flow path; and
 - Shape of the orifice.



Approach- need to compare baseline and project emissions

- Assume natural gas and air have same energy loss, so substitute C_v for air into (1)

$$Q_{CH_4} = Q_{AIR} * \frac{1}{\sqrt{\frac{1}{G_{AIR}}}} * \frac{1}{Y_{AIR}} * Y_{CH_4} * \sqrt{\frac{1}{G_{CH_4}}}$$

- Substituting terms

$$Q_{CH_4} = Q_{AIR} * \sqrt{\frac{G_{AIR}}{G_{CH_4}}} * \frac{1 - \frac{x}{\left(\frac{1 - (0.41 + 0.35 * \beta^4) * (x/k_{CH_4})}{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)} \right) * x_T}}{1 - \frac{x}{\left(\frac{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)}{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)} \right) * x_T}}$$

- k =specific heat of gas; G =specific gravity of gas; β = orifice to pipe diameter ration



Equations to quantify emissions

■ CH₄

$$Q_{CH_4} = Q_{AIR} * \sqrt{\frac{G_{AIR}}{G_{CH_4}}} * \frac{1 - \frac{x}{\left(\frac{1 - (0.41 + 0.35 * \beta^4) * (x/k_{CH_4})}{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)} \right) * x_T}}{1 - \frac{x}{\left(\frac{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)}{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)} \right) * x_T}} * \%CH_4 * \rho_{CH_4}$$

■ CO₂

$$Q_{CH_4} = Q_{AIR} * \sqrt{\frac{G_{AIR}}{G_{CH_4}}} * \frac{1 - \frac{x}{\left(\frac{1 - (0.41 + 0.35 * \beta^4) * (x/k_{CH_4})}{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)} \right) * x_T}}{1 - \frac{x}{\left(\frac{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)}{1 - (0.41 + 0.35 * \beta^4) * (x/1.4)} \right) * x_T}} * \%CH_4 * \rho_{CH_4} * \frac{\%CO_2}{\%CH_4} * \frac{44}{16}$$